Pilot Plant Testing of Piperazine (PZ) with Advanced Flash Regeneration

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# **Advanced Flash Stripper (AFS)**



# **New Equipment on Skid**



# Outline

- Funding and objectives : NCCC fall 2017
- Capital and Energy << MEA</li>
- Solvent Management of PZ Prepared

# **Project Budget (\$million)**

	BP1	BP2	Total
Federal	1.6	3.3	5.2
Cost Share	1.1	0.3	1.5
Total	2.7	3.6	6.7

Cost share by CO<sub>2</sub> Capture Pilot Plant Project (C2P3)



# **Objective is to develop PZ with advanced regeneration at 150°C**

PZ	<ul> <li>Optimize solvent (8m vs 5m)</li> <li>Demonstrate resistance to oxidation, nitrosation, &amp; corrosion</li> </ul>
Regeneration	<ul> <li>Two stage flash (2SF)</li> <li>Advanced flash stripper (AFS)</li> </ul>
Aerosols	<ul><li>Formation and control</li><li>Characterization</li></ul>

### Phased testing at UT SRP and NCCC to optimize PZ absorption/regeneration





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# Our test window: Fall 2017 parametric Spring 2018 long-term

		2017											2018																				
Activity	J	an	F	eb	М	ar	A	pr	М	ay	JL	In	Jl	l	Au	Jg	Se	ер	0	ct	Ν	0V	De	ec	Já	an	Fe	eb	Ma	ar	Ą	or	May
Skid Installed																																	
Water Test																																	
Commissioning																																	
Start-Up																																	
Parametric Field Campaign																																	
Long-term Field Campaign																																	
Site Restoration																																	
Analysis/Reporting																																	

## Advanced amine scrubbing gives 50% efficiency Limited by capital-energy tradeoff



### AFS also works with other solvents

	kg'	W <sub>eq</sub> (kJ/mol CO <sub>2</sub> )							
Solvent	(10 <sup>-7</sup> mol/Pa-s-m <sup>2</sup> )	Simple stripper	AFS						
7m MEA	4.3	36.3	32.7						
10m DGA	3.6	37.0	34.2						
8m PZ	8.5	34.9	31.4						
5m PZ	11.3	36.5	32.3						
2m PZ /3m HMPD	10.1	34.9	31.0						
•	$Rich P_{CO_2}^* = 5  kPa, Lec$	$an P_{CO_2}^* = 0.2 \ kPa$	0.175						

• Optimum cross exchanger 
$$\Delta T_{LM} = 5K \left(\frac{\mu}{\mu_{MEA}}\right)^{0.1}$$

#### AFS provides reversible stripper performance 90% removal, 0.24 lean ldg



#### **Possible long term conditions at NCCC** 0.24 lean ldg, 150°C/82 psia stripper, 2x20 ft absorber packing

CO <sub>2</sub> removal (%)	Gas Rate (MW)	Rich Ldg (mol CO2/eq PZ)	L/L <sub>min</sub>	W <sub>eq</sub> (kwh/tonne)	Q (GJ/tonne)
90	0.5	0.387	1.006	256	2.56
98.5	0.5	0.366	1.16	260	2.61
95.4	0.8	0.380	1.10	274	2.77

## **PZ losses and environmental impact**

- Resistant to corrosion, use more carbon steel
- Moderate volatility
  - Manage losses with water wash
  - Manage impurities with thermal reclaiming
- Manage aerosol with grow and capture
- Resistant to Degradation
  - –Thermally stable to 150°C
  - -Oxidation, 4x less than MEA
  - Nitrosation, decompose at 150°C
- Manage solid precipitation with rich storage

# **SRP Pilot Plant Corrosion 2017**

- Two ER corrosion probes in stripper
  - 316L SS
  - 1010 CS
- One ORP Probe
- In addition, one ER probe in absorber sump



### **SRP Pilot Plant Corrosion 2017**

Location	Alloy	T (°C)	Avg. Loading (mol CO <sub>2</sub> /mol N)	Corrosion (µm/yr)
Absorber	C1010	30	0.33	331
Stripper	C1010	150	0.21	325
Stripper	316L	150	0.21	174

• Absorber corrosion greater than expected

Corrosion (µm/yr)

**Good** 100 - 500

**Poor** 1000 - 5000

Unacceptable 5000+

• Low Fe<sup>2+</sup> solubility in PZ may result in FeCO<sub>3</sub> protective layer.





# **Oxidation Mitigation**

- Reaction w D.O.: 0.05 mmol/kg/cycle in HTOR
  - Minimize holdup at high temperature before stripper
  - Strip O<sub>2</sub> with N<sub>2</sub> mmol/(kg-cycle-mmol/kg Fe<sup>2+</sup>)
- Fe<sup>2+</sup> solubilized by degradation products
  - Oxidation  $\rightarrow$  Fe<sup>2+</sup> accumulation  $\rightarrow$  more oxidation
  - NO<sub>2</sub>  $\rightarrow$  MNPZ  $\rightarrow$  Oxidation in pilots w/ coal flue gas
    - Prescrub NO<sub>2</sub> and reclaim solvent to minimize Fe<sup>2+</sup>

### **Growth slows down at high part. number conc 5 m PZ, NCCC conditions**





### Baghouse at NCCC significantly reduced MEA emissions



# SO<sub>3</sub> Generation



### 10 to 30 ppm SO<sub>3</sub> usually not always produce aerosol



# Conclusions

- The Advanced Flash stripper will reduce  $W_{eq}$  by 10-20% for PZ and other solvents
- 5 m PZ is a superior solvent
  - Fast absorption, thermally stable, high P stripper
  - Good resistance to corrosion, oxidation
  - Managed aerosol

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